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## Effect of preparation methods on DeNOx efficiency of CeO<sub>2</sub>/TiO<sub>2</sub> catalysts

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**Abstract :** The DeNO<sub>x</sub> performance of catalysts is a key part in the selective catalytic reduction process. In this study,  $CeO_2/TiO_2$  catalysts were prepared by the impregnation method and the sol-gel method, and the DeNO<sub>x</sub> performance of the catalysts was tested on a self-built experimental system. The efficiency difference due to the two preparation methods was analyzed by X-ray diffraction technology and Brunauer-Emmett-Teller method. The experimental results showed that  $CeO_2/TiO_2$  catalysts prepared by the sol-gel method had a larger surface area and the DeNO<sub>y</sub> activity was

#### INTRODUCTION

The emission of nitrogen oxides during coal combustion is great harmful to the environment<sup>[1-3]</sup>. As an important part of nitrogen oxides removal technology, selective catalytic reduction (SCR) has been adopted in many power plants<sup>[4-6]</sup>. In SCR technology, the performance of the catalysts is the focus for researchers. Vanadium-titanium catalyst has received a lot of attention and been widely used in SCR technology, while the common method is to load  $V_2O_5$  on TiO<sub>2</sub> and add different amounts of WO<sub>3</sub> or MoO<sub>3</sub><sup>[7-10]</sup>. In addition, other metal oxides, such as Fe, Cu, Cr, and Mn, have been widely studied as active ingredients<sup>[11-13]</sup>. Feng Gao et al. studied the reaction kinetics of Cu-SSZ-13 catalysts with various Cu loadings<sup>[14]</sup>. The adhesion and surface characteristics of monolithic Cr-V/TiO<sub>2</sub>/ cordierite catalysts were investigated for lowtemperature NH<sub>3</sub>-SCR reactions by Hai-feng Huang et al.<sup>[15]</sup>.

Although the research for the effect of different

higher than the catalysts prepared by the impregnation method, when the temperature was below 350 °C. For  $\text{CeO}_2/\text{TiO}_2$  catalysts prepared by the impregnation method, the crystal form of  $\text{CeO}_2$  could be seen, when  $\text{CeO}_2$  content was 10%. However, if  $\text{CeO}_2$  content was more than 3%, the catalyst had relative high activity suitable for industrial application.

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loadings on SCR catalysts has been carried out for years, little work has been done to study the effect of preparation methods on the DeNOx efficiency. In this study,  $CeO_2/TiO_2$  catalysts were prepared by the impregnation (IM) method and the sol-gel (SG) method, and different amounts of CeO<sub>2</sub> were loaded in TiO<sub>2</sub> to determine the optimal loading amount of active substance. The microstructure of the catalysts was investigated to explore the reasons for the differences of DeNOx performance by X-ray diffraction (XRD) technology and Brunauer-Emmett-Teller (BET) method.

#### **EXPERIMENTAL SECTION**

#### **Experimental system**

The experimental system is as shown in Figure 1. In the experiments, the mixed gas of NO,  $O_2$  and  $N_2$  was simulated flue gas,  $NH_3$  was used as a reducing agent, wherein the NO content was 500 ppm, the same as  $NH_3$ .  $O_2$  content was about 4%, and  $N_2$  was used

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as the balance gas. There were three parts in the experimental system: the gas supply system, the reaction

system and the measurement system. The gas supply system provided simulated flue gas and reducing agent, and the gas flow was controlled by mass flow meter. The reaction system contained the reactor and temperature controller. As one-dimensional tube furnace, the reactor was made from quartz glass, filled with cotton insulation. The catalysts loaded in the reactor and were fixed by mullite asbestos in the position, in which a thermocouple was set to monitor temperature. The measurement system was mainly composed of flue gas analyzer (GASMET FTIR Dx4000), which was applied to record the concentration of NO and NH<sub>3</sub>.

### **Catalyst preparation**

The methods of catalyst preparation in the laboratory are mainly sol-gel method, precipitation method, ion exchange method and impregnation method. By Isometric impregnation method solution can just immerse all carrier particles to avoid the recovery steps of filtering and impregnating solution. In this work,  $CeO_2/TiO_2$  catalysts was prepared by IM method. Preparation process of granular  $CeO_2/TiO_2$  catalysts is shown in Figure 2.

Step-by-step SG preparation method is as follows: (1) Take appropriate amount of butyl titanate and

anhydrous ethanol (volume ratio is 4:1), then mix and stir fully to give a uniform and transparent light yellow solution, which is denoted by solution A.

- (2) Take a suitable amount of deionized water, ethanol, nitric acid (volume ratio is 1:1:0.2) and weigh a certain amount of cerium nitrate. Then mix the above solution, dissolve cerium nitrate and stir sufficiently to give a solution, which is denoted by solution B. And then different amounts of cerium nitrate can produce different  $CeO_2/TiO_2$  catalysts supporting different amount of  $CeO_2$ .
- (3) Place solution B in a water bath of magnetic stirrer and control a certain water bath temperature and stirring speed, at the same time drip the solution A through the burette slowly into the solution B to form a mixed solution that can hydrolyze. After dripping the solution A, stirring is continued for a period of time to give a pale yellow transparent sol and finally become wet gel.
- (4) Put wet gel in drying oven under 110 °C for 24 h, calcine in the muffle furnace for 5 h under 500 °C and fresh CeO<sub>2</sub>/TiO<sub>2</sub> catalyst is prepared. Finally, the catalyst is milled to 40 to 60 mesh to test its DeNOx efficiency.

The catalysts was named Cex/Ti(IM) or Cex/Ti(SG) in this study, and x means the mass percentage of CeO<sub>2</sub> in the catalyst.



Figure 2 : Preparation process of granular CeO<sub>2</sub>/TiO<sub>2</sub> catalysts by IM method

#### **RESULTS AND DISCUSSION**

#### DeNOx of CeO<sub>2</sub>/TiO<sub>2</sub> catalysts

Figure 3 shows that DeNOx efficiency of CeO<sub>2</sub>/ TiO<sub>2</sub> catalysts prepared by IM method versus temperature. As can be seen from the Figure 3, when CeO<sub>2</sub> content was between 0.5% and 2%, the DeNOx efficiency of CeO<sub>2</sub>/TiO<sub>2</sub> catalysts was relatively low. When CeO<sub>2</sub> content was 5% and 10%, CeO<sub>2</sub>/TiO<sub>2</sub> catalyst DeNOx efficiency was significantly high, and under 250 °C the DeNOx efficiency reached more than 93.4%. When CeO<sub>2</sub> content was 0.5%, in the temperature range of 200-300 °C the DeNOx efficiency was very low (between 9.7%-14.9%); under 350 °C and 400 °C the DeNOx efficiency was significantly increased to 48.1% and 98.9%. When CeO<sub>2</sub> content was 1%, the DeNOx efficiency had the same rules with Ce0.5/Ti (IM), the DeNOx efficiency increased slightly. Thus, the CeO<sub>2</sub>/TiO<sub>2</sub> catalysts DeNOx efficiency had a great relationship with CeO<sub>2</sub> content.

Figure 4 shows that DeNOx efficiency of CeO<sub>2</sub>/ TiO<sub>2</sub> catalysts prepared by SG method versus temperature. As can be seen from Figure 4, compared with Ce0.5/Ti-4 (IM), the DeNOx efficiency of CeO<sub>2</sub>/ TiO<sub>2</sub> catalysts was generally low when CeO<sub>2</sub> content is 0.5% below 400 °C. But when the temperature is higher than 400 °C, the efficiency greatly improved, and the



Figure 3 : DeNOx efficiency of CeO<sub>2</sub>/TiO<sub>2</sub> catalyst prepared by IM method



Figure 4 : DeNOx efficiency of CeO<sub>2</sub>/TiO<sub>2</sub> catalyst prepared by SG method

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efficiency is 82.1%. When  $\text{CeO}_2$  content continued to increase, the catalyst activity under low temperature continued to grow, but the catalyst DeNOx efficiency from different CeO<sub>2</sub> content decreased in the temperature range of 350-450 °C and both efficiency remained above 76.2%.

#### Microscopic properties of catalysts

The catalysts with different cerium contents were prepared in the experiments, by IM method and SG method. The specific surface area, pore volume, and pore diameter were listed in detail in TABLE 1. We can find that by SG method Ce3/Ti(SG) has a higher specific surface area of 97.211m<sup>2</sup>/g, while Ce3/Ti(IM) has specific surface area of 74.520 m<sup>2</sup>/g.

catalyst	Specific surface area (m <sup>2</sup> /g)	Pore volume (ml/g)	Pore diameter (nm)
Ce3/Ti(IM)	74.520	0.017	18.194
Ce3/Ti(SG)	97.211	0.027	19.237

Figure 5 shows that three kinds of XRD patterns of  $CeO_2/TiO_2(IM)$  catalysts, of which  $CeO_2$  accounted for 0.5%, 3% and 10%. As can be seen from the figure, if the  $CeO_2$  content increased from 0.5% to 3%, the diffraction peak position on the XRD patterns did not change significantly. However, the intensity of the characteristic peak became slightly smaller, indicating in  $CeO_2/TiO_2(IM)$  CeO<sub>2</sub> and TiO<sub>2</sub> were better together and TiO<sub>2</sub> grains of catalysts were smaller. All the catalysts only appeared anatase TiO<sub>2</sub> characteristic peaks, and no CeO<sub>2</sub> crystal phase, indicating that when



Figure 5 : XRD pattern of CeO<sub>2</sub>/TiO<sub>2</sub> catalysts prepared by IM method

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CeO<sub>2</sub> content was less than 3%, cerium was well dispersed on the surface. There was CeO<sub>2</sub> characteristic diffraction peaks ( $2\theta$ =28.555°, 33.082°) in Ce10/Ti-4 (IM), indicating CeO<sub>2</sub> grains appeared in the catalyst and CeO<sub>2</sub> loading exceeded the saturation value of CeO<sub>2</sub> in the TiO<sub>2</sub> surface. CeO<sub>2</sub> grain is not active for SCR reaction, so it should be avoided in the preparation process.

Figure 6 shows that three kinds of XRD patterns of  $CeO_{2}/TiO_{2}(SG)$ , of which  $CeO_{2}$  accounted for 0.5%, 3% and 10%. As can be seen from the figure, when  $CeO_2$  content was 0.5%, we can observe obvious anatase TiO<sub>2</sub> characteristic peaks, rutile TiO<sub>2</sub> diffraction peaks ( $2\theta=27.508^\circ$ , 36.159°) and brookite TiO<sub>2</sub> characteristic peaks, indicating that when catalyst was prepared by SG method, the TiO<sub>2</sub> appeared more changing. When  $\text{CeO}_2$  content was 3%, the peak shape of anatase TiO<sub>2</sub> became incomplete, broad and diffuse. When  $CeO_2$  content increased to 10%, the peak shape was more broad and low, indicating that the electronic interaction between CeO<sub>2</sub> and TiO<sub>2</sub> strengthened, and CeO<sub>2</sub> was dissolved in TiO<sub>2</sub> with highly dispersed or amorphous state. Meanwhile, rutile TiO<sub>2</sub> peaks disappeared, but brookite TiO<sub>2</sub> still existed with lower intensity. All these indicated the increase of CeO<sub>2</sub> content suppressed the transformation from anatase TiO<sub>2</sub> to rutile TiO<sub>2</sub>.



Figure 6 : XRD pattern of CeO<sub>2</sub>/TiO<sub>2</sub> catalysts prepared by SG method

#### CONCLUSIONS

The specific surface area is an key factor that affected the DeNOx efficiency. The catalysts based on

 $CeO_2/TiO_2$  made by SG method have greater specific surface area. XRD shows that the rutile and broolnte type of TiO<sub>2</sub> appeared in the catalysts prepared by SG method and the crystal form of CeO<sub>2</sub> did not show up. The crystal form of CeO<sub>2</sub> appeared as the concentration of CeO<sub>2</sub> was 10% in the catalysts prepared by IM method. It demonstrated that CeO<sub>2</sub> was not well dispersed on the surface of the carrier.

The CeO<sub>2</sub>/TiO<sub>2</sub> catalysts prepared by IM method have relatively high DeNOx efficiency when the concentration of CeO<sub>2</sub> was 3% and that activity will not decline within a temperature range of 350-400 °C. The DeNOx efficiency of CeO<sub>2</sub>/TiO<sub>2</sub> catalysts prepared by SG method turned out a litthle higher than that prepared by IM method when the temperature was below 350 °C.

#### REFERENCES

- J.S.Gaffney, N.A.Marley; Atmos.Environ, 43(1), 23-36 (2009).
- [2] K.Skalska, J.S.Miller, S.Ledakowicz; Sci.Total Environ, 408(19), 3976-3989 (2010).
- [3] M.T.Izquierdo, B.Rubio, C.Mayoral, J.M.Andres; Fuel, 82(2), 147-151 (2003).

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- [4] I.Malpartida, O.Marie, P.Bazin, M.Daturi, X.Jeandel; Appl.Catal.B, 113, 52-60 (2012).
- [5] W.D.Fan, Z.C.Lin, Y.Y.Li, Y.Li; Energy Fuels, 24(3), 1573-1583 (2010).
- [6] P.Forzatti, L.Lietti; Catal. Today, 155(1-2), 131-139 (2010).
- [7] S.T.Choo, Y.G.Lee, I.S.Nam, S.W.Ham, J.B.Lee; Appl.Catal A, 200(1–2), 177-188 (2000).
- [8] J.Arfaoui, L.K.Boudali, A.Ghorbel, G.Delahay; Catal. Today, 142(3-4), 234-238 (2009).
- [9] M.Kobayashi, K.Miyoshi; Appl.Catal.B, 72(3–4), 253-261 (2007).
- [10] K.Bourikas, C.Fountzoula, C.Kordulis; Langmuir, 20(24), 10663-10669 (2004).
- [11] A.Sultana, M.Haneda, T.Fujitani, H.Hamada; Catal.Lett., 114(1-2), 96-102 (2007).
- [12] M.Kobayashi, R.Kuma, A.Morita; Catal.Lett., 112(1-2), 37-44 (2006).
- [13] G.Busca, L.Lietti, G.Ramis, F.Berti; Appl.Catal.B, 18(1-2), 1-36 (1998).
- [14] F.Gao, E.D.Walter, E.M.Karp, J.Y.Luo, R.G.Tonkyn, J.H.Kwak, J.Szanyi, C.H.Peden; J.Catal., 300, 20-29 (2013).
- [15] H.F.Huang, L.L.Jin, H.F.Lu, H.Yu, Y.J.Chen; Catal.Commun., 34(5), 1-4 (2013).